

Viscosity

Viscosity (η) → property of a liquid or gas in which one layer opposes the flow of adjacent layer.
 i.e. Two layers oppose their relative motion.

unit of ' η '
 1 decapoise = 10 poise
 S.I → poiseuille
 C.G.S → poise

Dimension of ' η '
 $[ML^{-1}T^{-1}]$

General properties →

- ii) → With rise in density, viscosity of liquid increase but that of gas decrease.
- *** iii) → With rise in temp., viscosity of liq ↓, but that of gas ↑.
- *** iii) → With rise in pressure, viscosity of liq ↑, but that of gas is independent of pressure.
- iv) → In case of water with rise in pressure viscosity ↓.
- *** iv) → Rate of change of speed $w \cdot r$ + distance measured in perpendicular direction of flow is dv/dy & called velocity gradient.

$$P + \frac{1}{2} \rho v^2 + \rho gh = \text{const} = K$$

$$\frac{P}{\rho g} + \frac{v^2}{2g} + h = \frac{K}{\rho g}$$

\downarrow Press. head \downarrow velo. head \downarrow pot. energy head.

Viscous force = $F \propto A$
 $\propto \frac{dv}{dy}$

$$F \propto A \frac{dv}{dy} \Rightarrow F = -\eta A \frac{dv}{dy}$$

η → coefficient of viscosity.
 $\frac{dv}{dy}$ → velocity gradient.

opposing nature of viscous force.

*** AIIMS 2016 *** Poiseuille formula -

Rate of flow of liquid with respect to time. i.e. volume flow in persecond. through a capillary tube of radius 'R', length 'L', when a pressure difference 'p' is applied is given by -

$$Q = \frac{\pi P R^4}{8 \eta L}$$

L → Length of cap.

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Stoke's Law

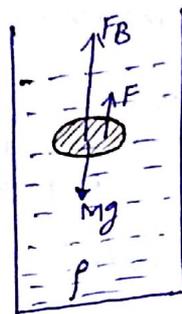
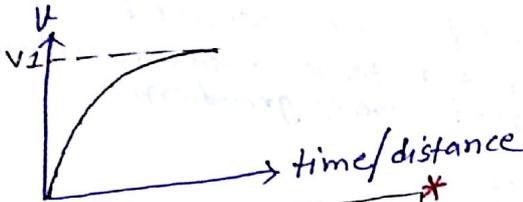
When force acting on a sphere of radius 'r' moving in liquid with speed 'v' -

$$F = 6\pi\eta r v$$

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Terminal velocity →

When a spherical object of radius 'r', density 'σ' fall in a liquid of density ρ then 1st velocity ↑ After some time net force on it becomes zero. so, velocity become const. called terminal velocity.



$$a = \frac{(\rho_s - \rho_l) - \frac{9\eta v}{2r^2 \rho_s}}{\rho_s}$$

$$V_T = \frac{2}{9} \frac{r^2 (\sigma - \rho) g}{\eta}$$

If 'n' identical sphere of same material are moving in a liquid with const. speed 'v' are calapsed to form a single sphere, the new const. speed will be.

$$V_T = \frac{2}{9} \frac{(\rho_s - \rho_l) r^2 g}{\eta}$$

$$V_T \propto r^2$$

$$V_T' \propto R^2$$

$$\frac{V_T'}{V_T} = \left(\frac{R}{r}\right)^2$$

$$R = n^{1/3} \cdot r$$

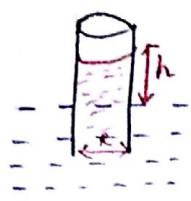
$$\frac{R}{r} = n^{1/3}$$

$$\frac{V_T'}{V_T} = n^{2/3}$$

$$\therefore V_T' = n^{2/3} V$$

- iii → Find the rise of liquid level in capillary tube.
- ii → Find Work done by surface tension in this process.
- ii → Find the ΔU in gravitational pot. energy in this process
(Assume contact angle is zero)

iii → $h = \frac{2\sigma}{\rho g R}$ or, $h = \frac{2\sigma}{\rho g d}$



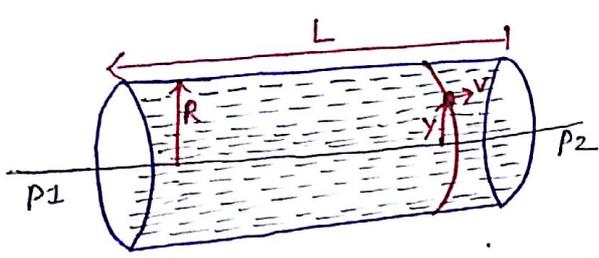
ii → $W_T = \sigma \times 2\pi R \times \frac{2\sigma}{\rho g R}$

$W_T = \frac{4\pi\sigma^2}{\rho g}$

ii → $\Delta U_g = mgh$

$\rho \times \pi R^2 h \times g \times \frac{h}{2}$
 $= \frac{\rho g \cdot \pi R^2 \times 4\sigma^2}{2 \rho^2 g^2 R} = \frac{2\pi\sigma^2}{\rho g}$

$W_T = \Delta U_g = \frac{2\pi\sigma^2}{\rho g}$

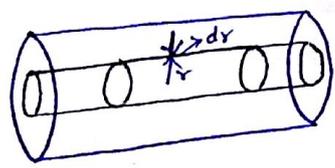


$v = \frac{P}{4\eta L} (R^2 - y^2)$
 $P = P_1 - P_2$

* At $y = 0 \Rightarrow v = v_{max} = v_0$
 $v_0 = \frac{PR^2}{4\eta L}$

* At $y = R \Rightarrow v = v_{min} = 0$

→



Diff. in K.E = $\pi \rho L \cdot v \cdot dr \left[\frac{P}{4\eta L} (R^2 - r^2) \right]^2$

$m_0 = \rho \times \pi R^2 L$
 $K = \frac{1}{2} m_0 v_{avg}^2$

$K = \frac{\pi \rho R^6}{96 \eta^2 L} P^2 \Rightarrow$ Total K.E in pipe.